



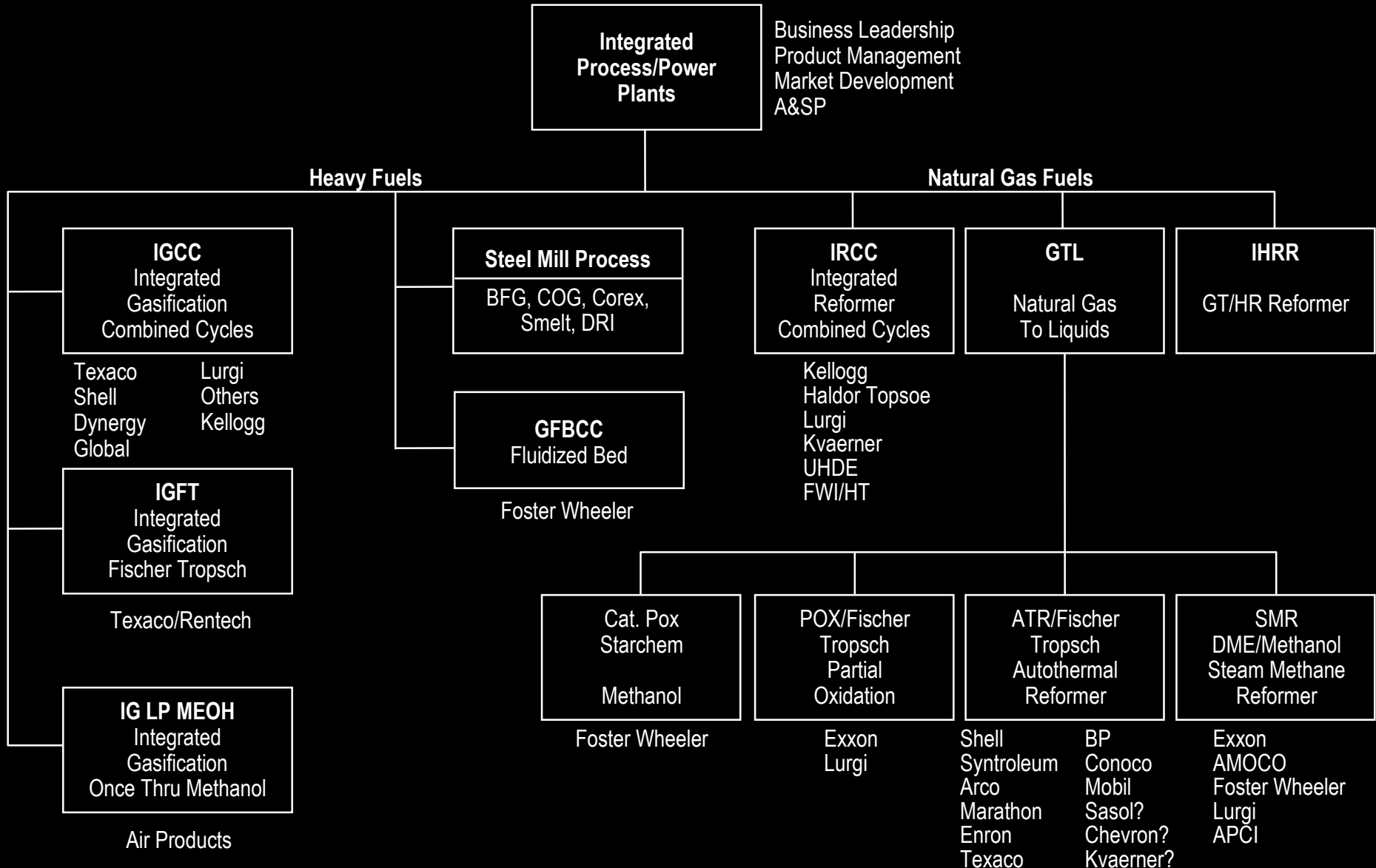
GE Power Systems

Hydrogen Workshop

*Douglas M. Todd
GE Schenectady, NY
September 19, 2000*

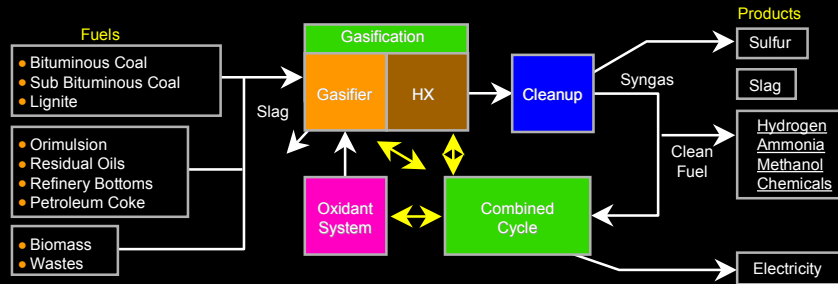


Process Power Plants



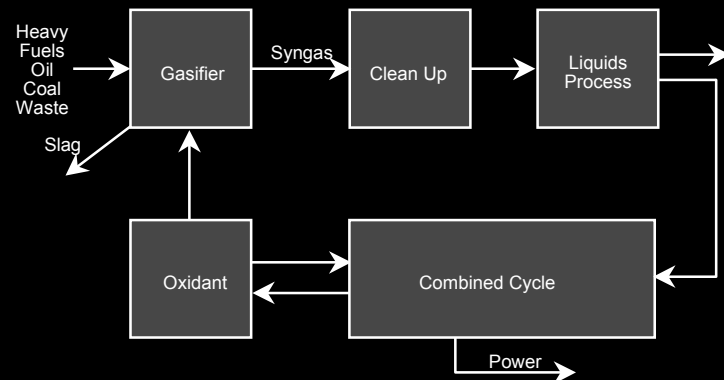
Process Power Plants Examples

IGCC



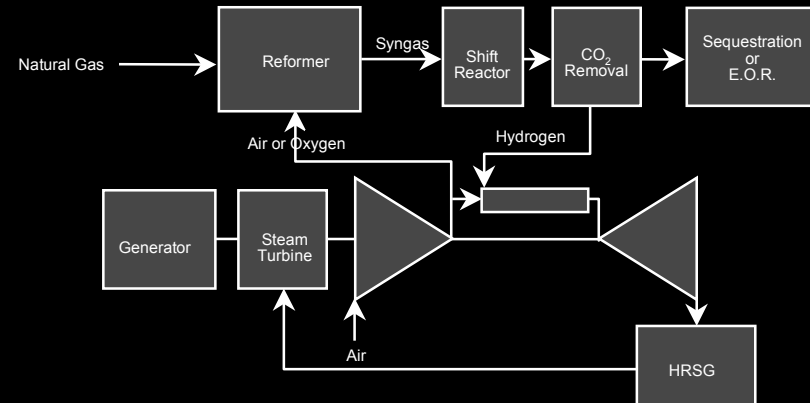
Clean Power From Heavy Fuels

IGFT / Methanol



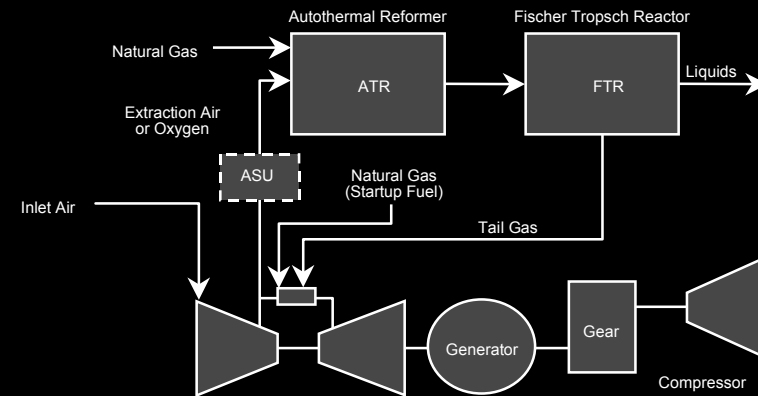
Enhanced IGCC Economics

IRCC



CO₂ Reduction

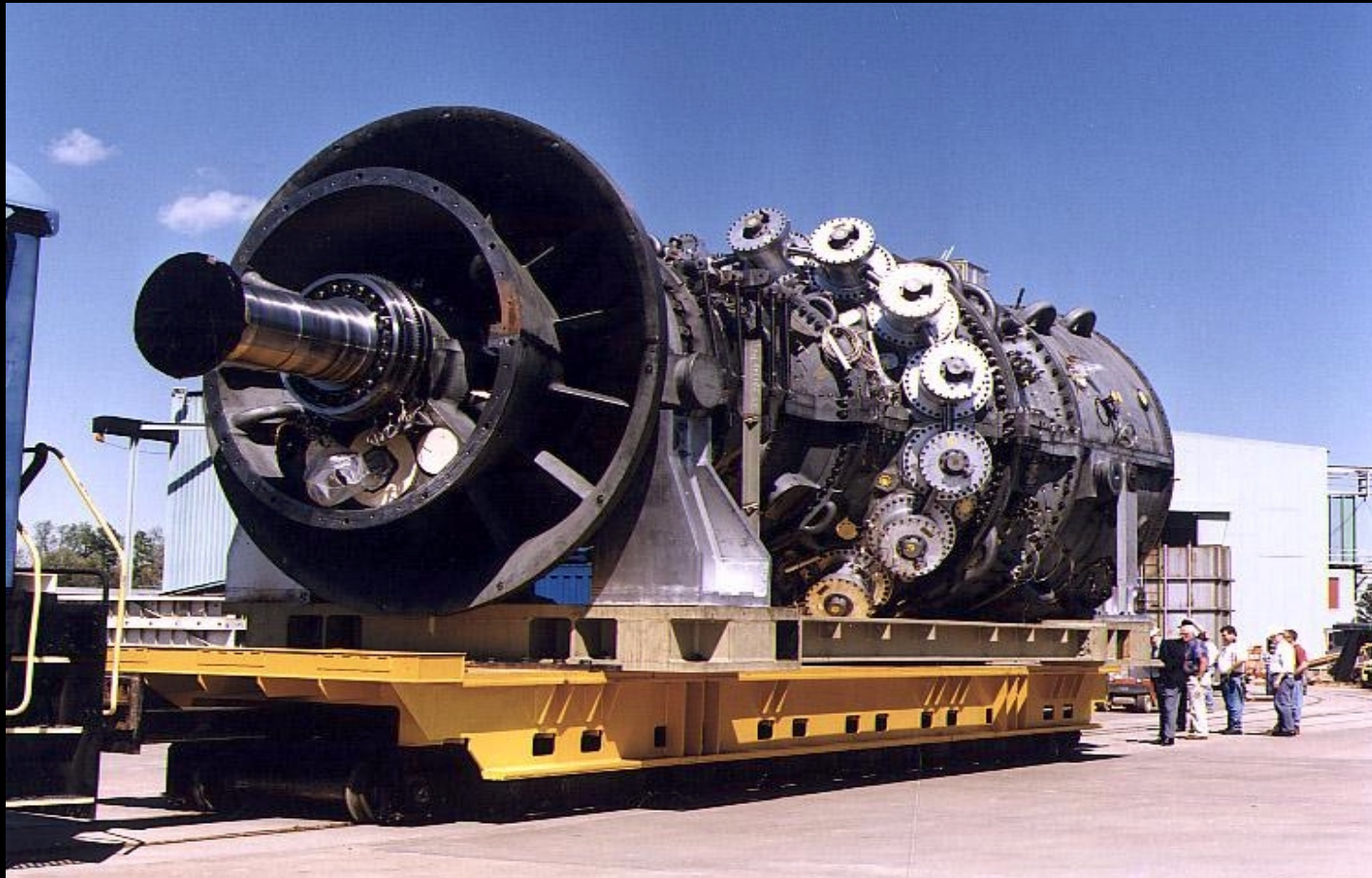
GTL



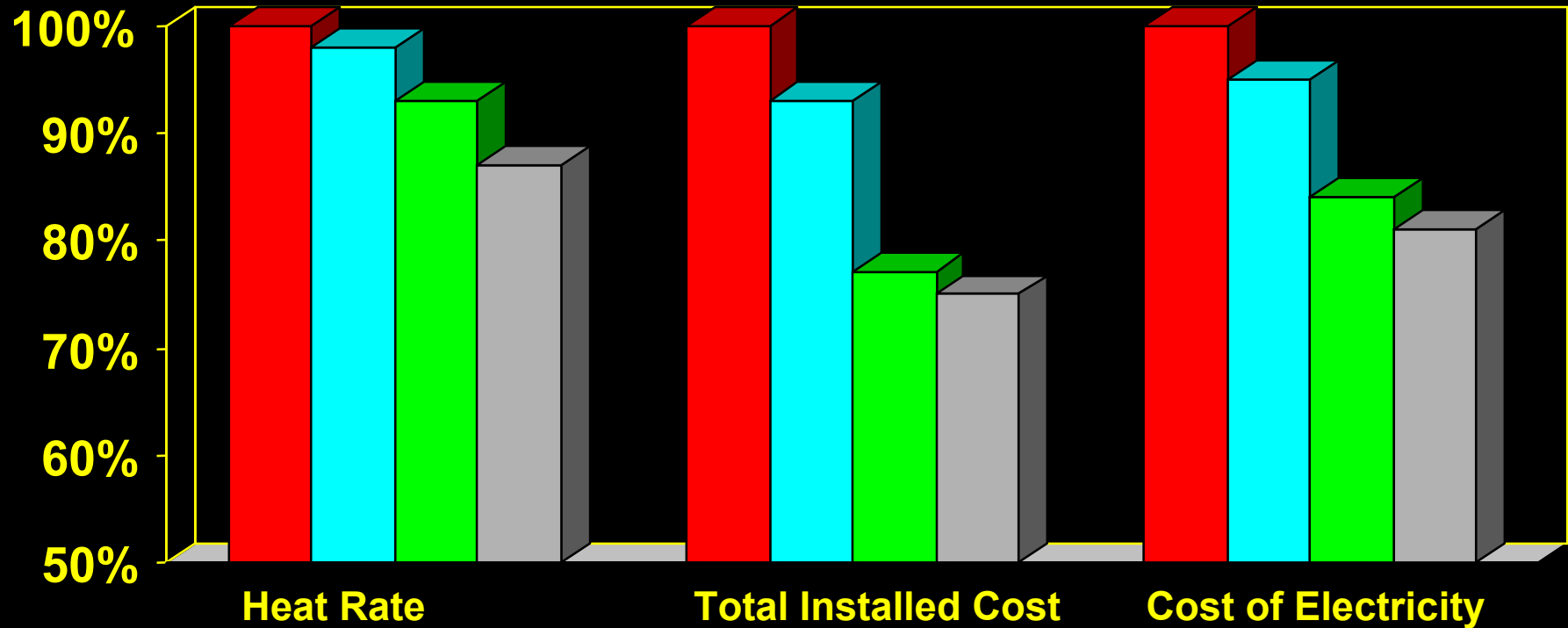
Monetizing Remote Gas

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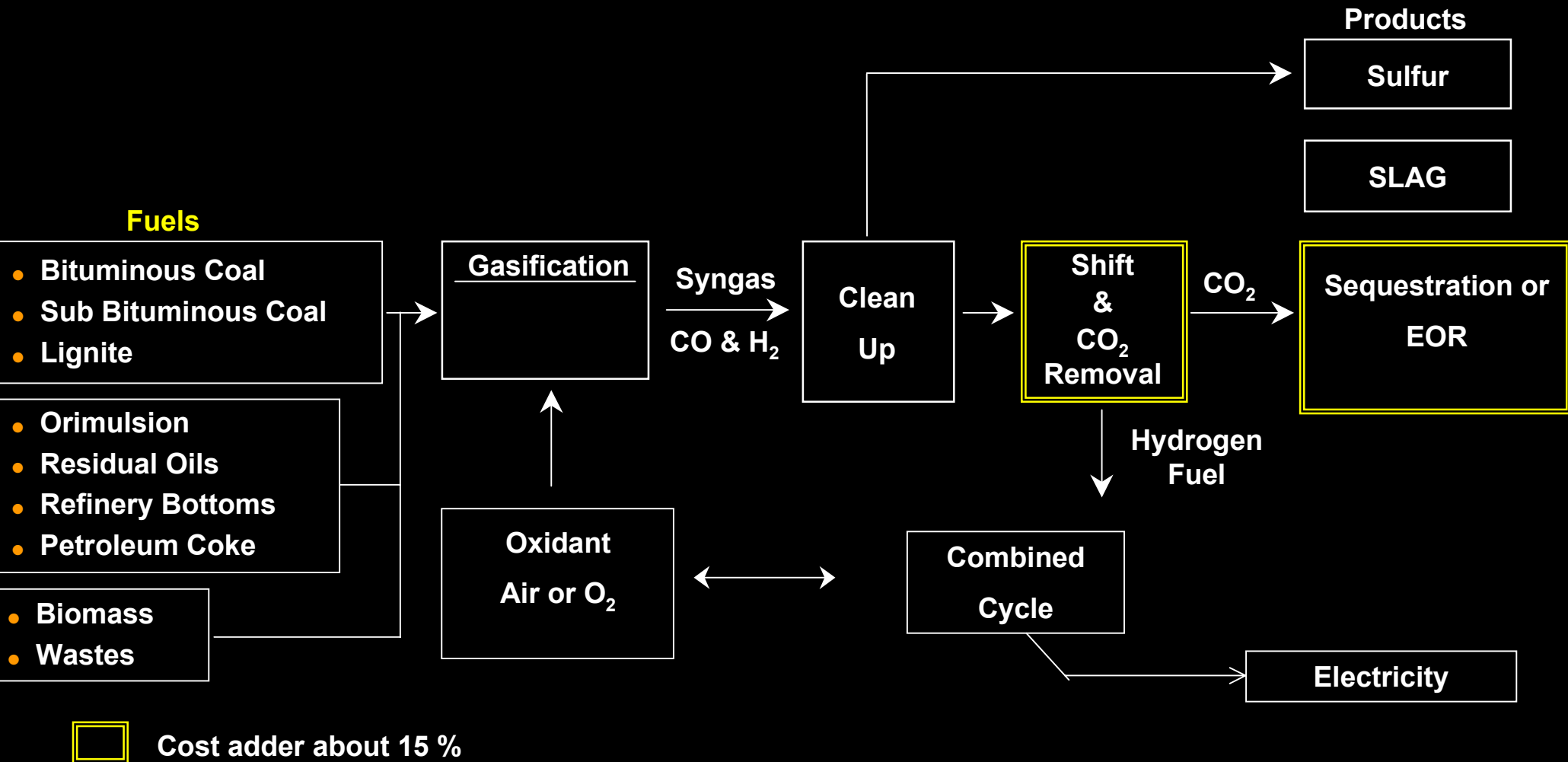
GE's MS9001H Gas Turbine



Economic Impact of HEQ IGCC Design Study Improvements



■ 1994 9F HEQ ■ 1999 9H HEQ
■ 1997 9FA HEQ ■ 1999 9H HR Oil



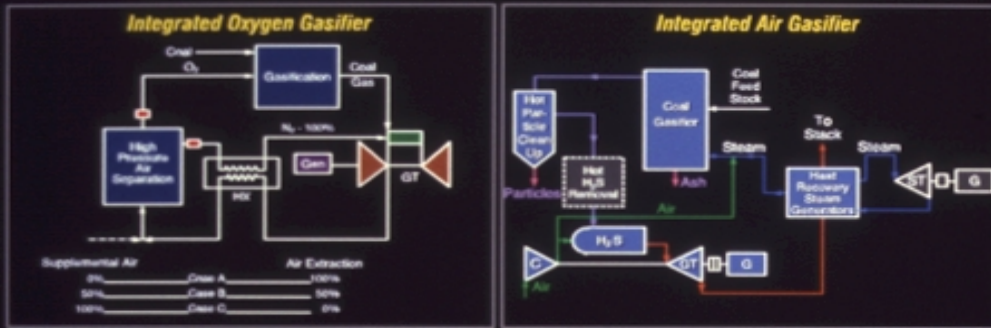
CO₂ Emission Reduction for Heavy Fuel Power Plants

IGCC Penetration

<u>Customer</u>	<u>C.O. Date</u>	<u>MW</u>	<u>Application</u>	<u>Gasifier</u>
SCE Cool Water - USA	1984	120	Power/Coal	Texaco - O₂
LGTI - USA	1987	160	Cogen/Coal	Destec - O ₂
Demkolec - Netherlands	1994	250	Power/Coal	Shell - O ₂
PSI/Destec - USA	1995	260	Repower/Coal	Destec - O₂
Tampa Electric - USA	1996	260	Power/Coal	Texaco - O₂
Texaco El Dorado - USA	1996	40	Cogen/Pet Coke	Texaco - O₂
SUV - Czech.	1996	350	Cogen/Coal	ZUV - O₂
Schwarze Pumpe - Germany	1996	40	Power/Methanol/Lignite	Noell - O₂
Shell Pernis - Netherlands	1997	120	Cogen/H₂/Oil	Shell - O₂
Puertollano - Spain	1998	320	Power/Coal/Pet Coke	Prenflow - O ₂
Sierra Pacific - USA	1998	100	Power/Coal	KRW - Air
ISAB - Italy	1999	500	Power/H ₂ /Oil	Texaco - O ₂
API - Italy	2000	250	Power/H ₂ /Oil	Texaco - O ₂
MOTIVA - Delaware	2000	240	Repower/Pet Coke	Texaco - O₂
Sarlux/Enron - Italy	2000	550	Cogen/H₂/Oil	Texaco - O₂
EXXON - Singapore	2002	180	Cogen/H₂/Oil	BGL - O₂
Bio Electrica - Italy	2000	180	Power/Biomass	Texaco - O₂
FIFE - Scotland	2000	12	Power/H₂/Cogen/Oil	Lurgi - Air
EDF - Total	2003	400	Power/Sludge	Texaco - O₂
FIFE Electric - Scotland	2003	400	Power/Coal/RDF	BGL - O₂
Nihon Sekiyu - Japan	2004	350	Power/Oil	Texaco - O ₂
IOC Paradip	2004	180	Power/Pet Coke	Shell - O₂
CONFIDENTIAL	2004	750	Power/Pet Coke	Texaco - O₂
PIEMSA	2004	800	Power/H₂/Oil	Texaco - O₂

GE IGCC Development Program

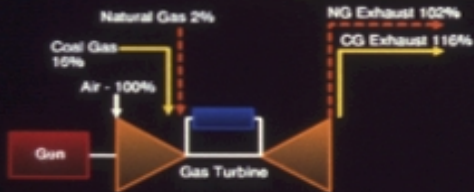
Systems



Combustion



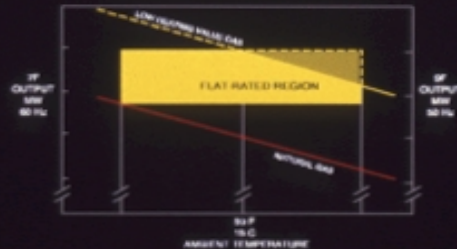
Rating Enhancements



- 14% Difference in Flow at Same Firing Temperature Makes 28% More Output (No Compression Power)

20% Extra Output

	GT	IGCC
- 6FA	- 90 MW	126 MW
- 7FA	- 200 MW	280 MW
- 9EC	- 215 MW	300 MW
- 9FA	- 300 MW	420 MW
- 7H	-	460 MW
- 9H	-	550 MW



Next Generation

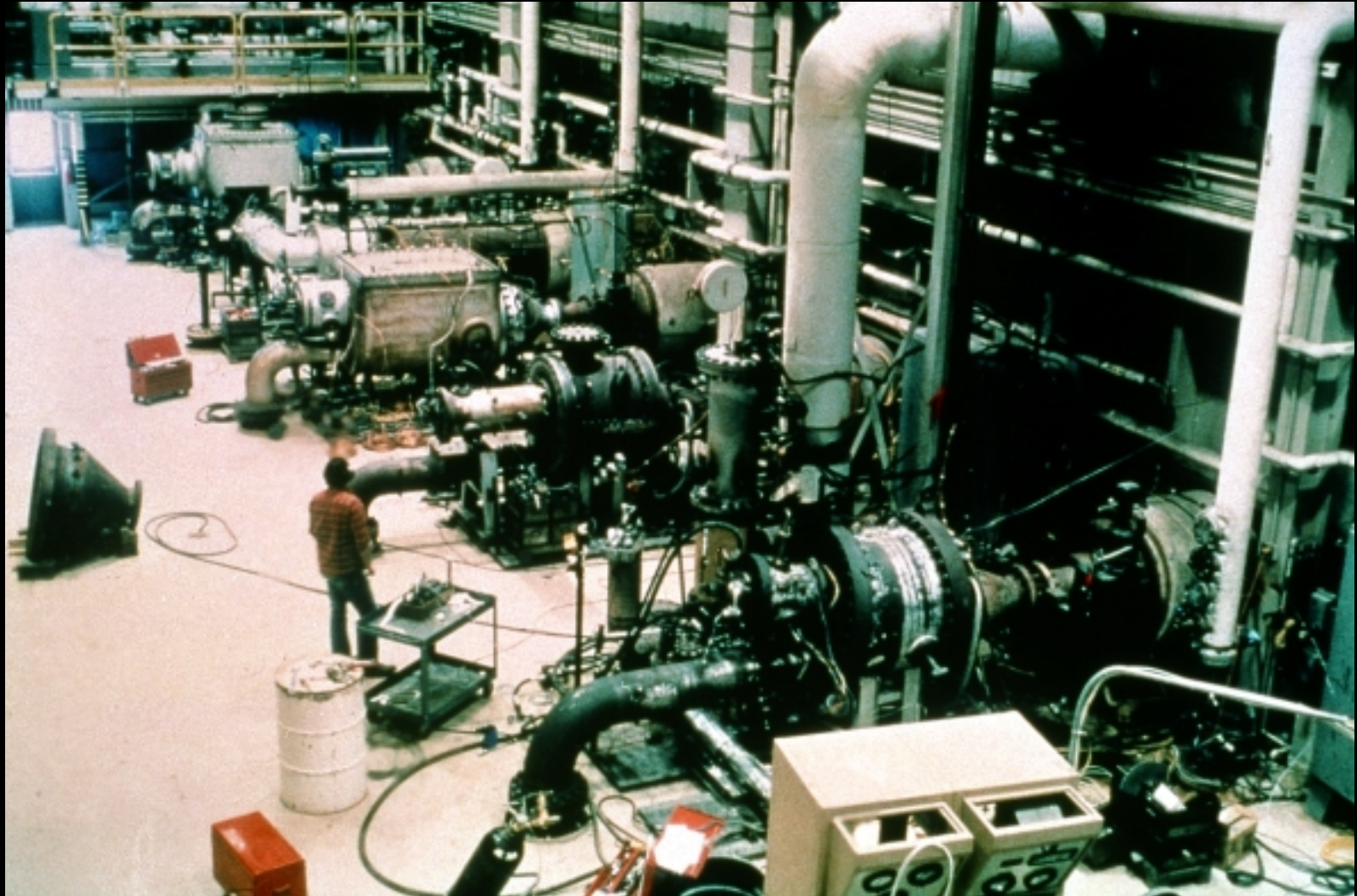


Single Train IGCC Plants

	S107H (60 Hz)	S109H (50 Hz)
Net Output	460 MW	550 MW
Thermal Eff.	50%	50%

GT24355

GE PGE Combustion Laboratory



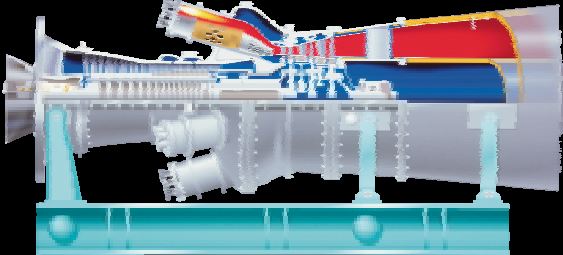
Syngas Comparison

<u>Syngas</u>	<u>PSI</u>	<u>Tampa</u>	<u>El Dorado</u>	<u>Pernis</u>	<u>Sierra Pacific</u>	<u>ILVA</u>	<u>Schwarze Pumpe</u>	<u>Sarlux</u>	<u>Fife</u>	<u>Exxon Singapore</u>	<u>Motiva Delaware</u>	<u>Confidential</u>	<u>PIEMSA</u>	<u>Tonghua</u>
H ₂	24.8	37.2	35.4	34.4	14.5	8.6	61.9	22.7	34.4	44.5	32.0	33.34	42.3	10.3
CO	39.5	46.6	45.0	35.1	23.6	26.2	26.2	30.6	55.4	35.4	49.5	42.44	47.77	22.3
CH ₄	1.5	0.1	0.0	0.3	1.3	8.2	6.9	0.2	5.1	0.5	0.1	0.06	0.08	3.8
CO ₂	9.3	13.3	17.1	30.0	5.6	14.0	2.8	5.6	1.6	17.9	15.8	17.76	8.01	14.5
N ₂ + AR	2.3	2.5	2.1	0.2	49.3	42.5	1.8	1.1	3.1	1.4	2.15	5.72	2.05	48.2
H ₂ O	22.7	0.3	0.4	--	5.7	--	--	39.8	--	0.1	0.44	0.08	0.15	0.9
LHV, - Btu/ft ³	209	253	242	210	128	183	317	163	319	241	248	230.4	270.4	134.6
- kJ/m ³	8224	9962	9528	8274	5024	7191	12,492	6403	12,568	9,477	9,768	9,079	10,655	5304
T _{fuel} F/C	570/300	700/371	250/121	200/98	1000/538	400/204	100/38	392/200	100/38	350/177	570/299	300/149	338/170	-
H ₂ /CO Ratio	.63	.80	.79	.98	.61	.33	2.36	.74	.62	1.26	.65	.79	.89	.46
Diluent	Steam	N ₂	N ₂ /Steam	Steam	Steam	--	Steam	Moisture	H ₂ O	Steam	H ₂ O/N ₂	N ₂ /H ₂ O	N ₂	n/a
Equivalent LHV														
- Btu/ft ³	150	118	113*	198	110	--	200	--	*	116	150	115.3	129	134.6
- kJ/m ³	5910	4649	4452	7801	4334	--	7880	--	--	4600	5910	4543	5083	5304

* Always co-fired with 50% natural gas

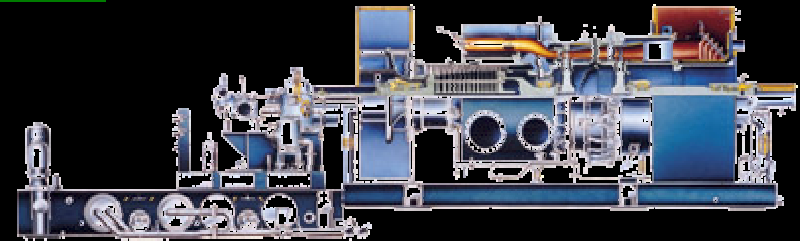
Combustion Technology Development

IGCC



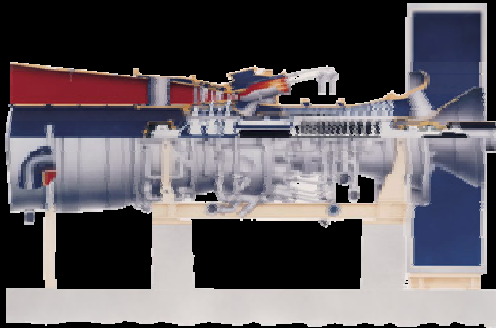
MOTIVA - First Pet Coke Appli. With 9 ppm NO_x
Exxon - 1st St. Cracker Bottoms With 25% Wobbe Var.

GTL



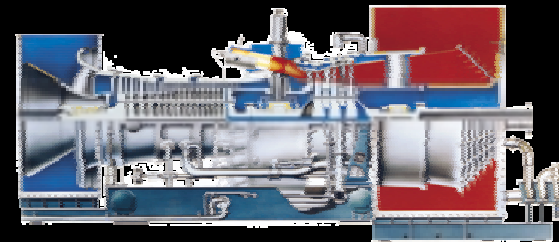
Air - First Air-Blown Tail Gas
Oxygen - Variety of Syngas

IRCC



Hydrogen Combustion for Reduction of CO₂

Steel



Mixtures of BFG, COG, Nat. Gas

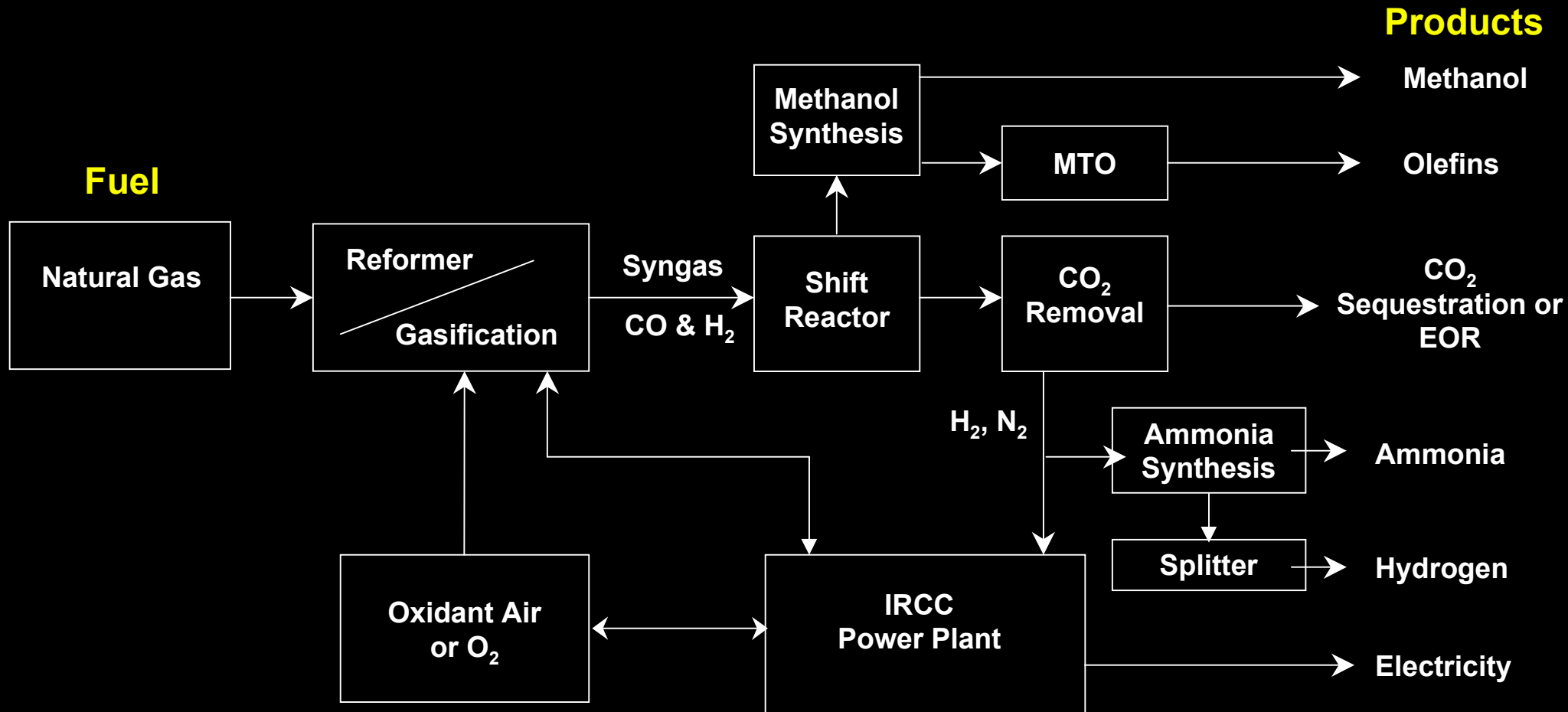
Shell-Pernis Coproduction Plant

- 1650 t/d Vacuum Residue
- 2 x 6B Gas Turbines
- Shell/Lurgi Gasifier
- 255 t/d Hydrogen
- 115 MW Power
- Steam to Refinery
- Operation 1997



RDC 27963

IRCC Electricity Coproduction



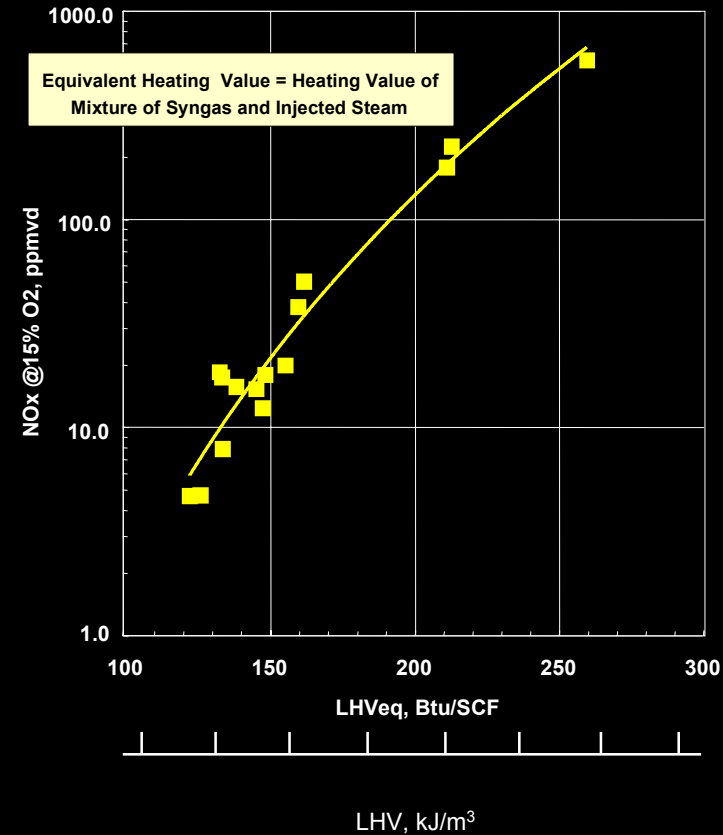
**Multiple Products and Electricity with
CO₂ Emmission Reduction from Natural Gas**

Combustion Test Objectives

- Evaluate Operability and Emissions of the GE IGCC Multi-Nozzle Combustor burning IRCC High H₂ Fuel
- Evaluate Component Metal Temperatures Throughout the Load Range
- Determine Sensitivity of Major Performance Parameters to Variations in Hydrogen Content

NO_x vs Equivalent Calorific Value for Several Fuel Compositions

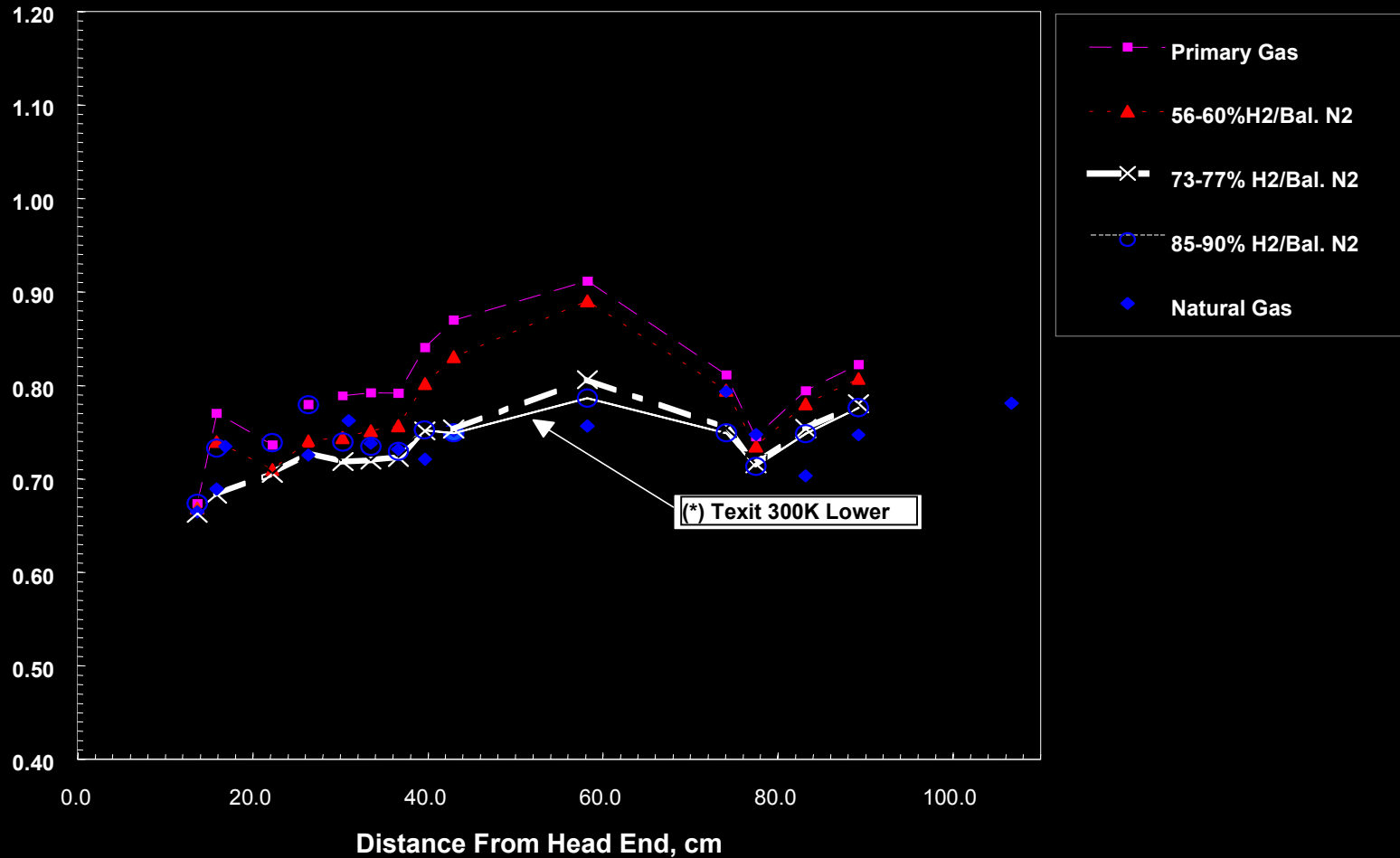
Video Capture of Flame Structure - 85-90% H₂



50 - 95% H₂ By Volume, Bal. N₂, N₂ + H₂O

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Combustor Metal Temperatures at 210° from TDC - Inline with Fuel Nozzles

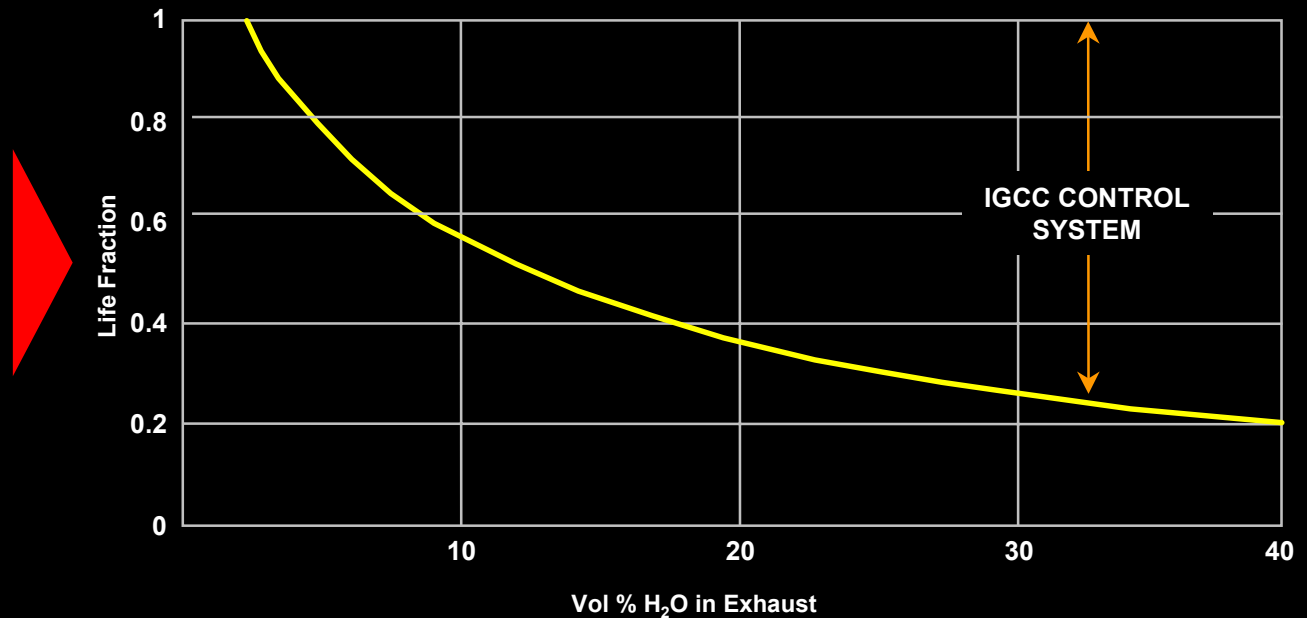


Effect of Fuel Composition on Axial Metal Temperature Distribution at 210° from TDC

Syngas - Reliability / Availability / Maintenance

Syngas Combined Cycle Can Have Same Performance as Natural Gas Combined Cycle

- Need Automatic Fuel Switch/Nitrogen Purge
- Need Clean Syngas
- Reduced Firing Temp to Maintain Design Metal Temp/ 100% Life



Conclusions

- Hydrogen is an acceptable fuel for GE Gas Turbines using IGCC Combustors
- NOx Emissions Below 10 ppmvd @15% O₂
- No Adverse Effects on Combustion Parts Lives
- Reliability, Availability and Maintainability Equivalent to NG
- Integration of a Hydrogen Fueled Gas Turbine with Process Plants is Technically Feasible to Reduce CO₂ Emissions by 90%
- Optimization Required to Improve Cost of Electricity