

g

GE Power Systems

Hydrogen Workshop

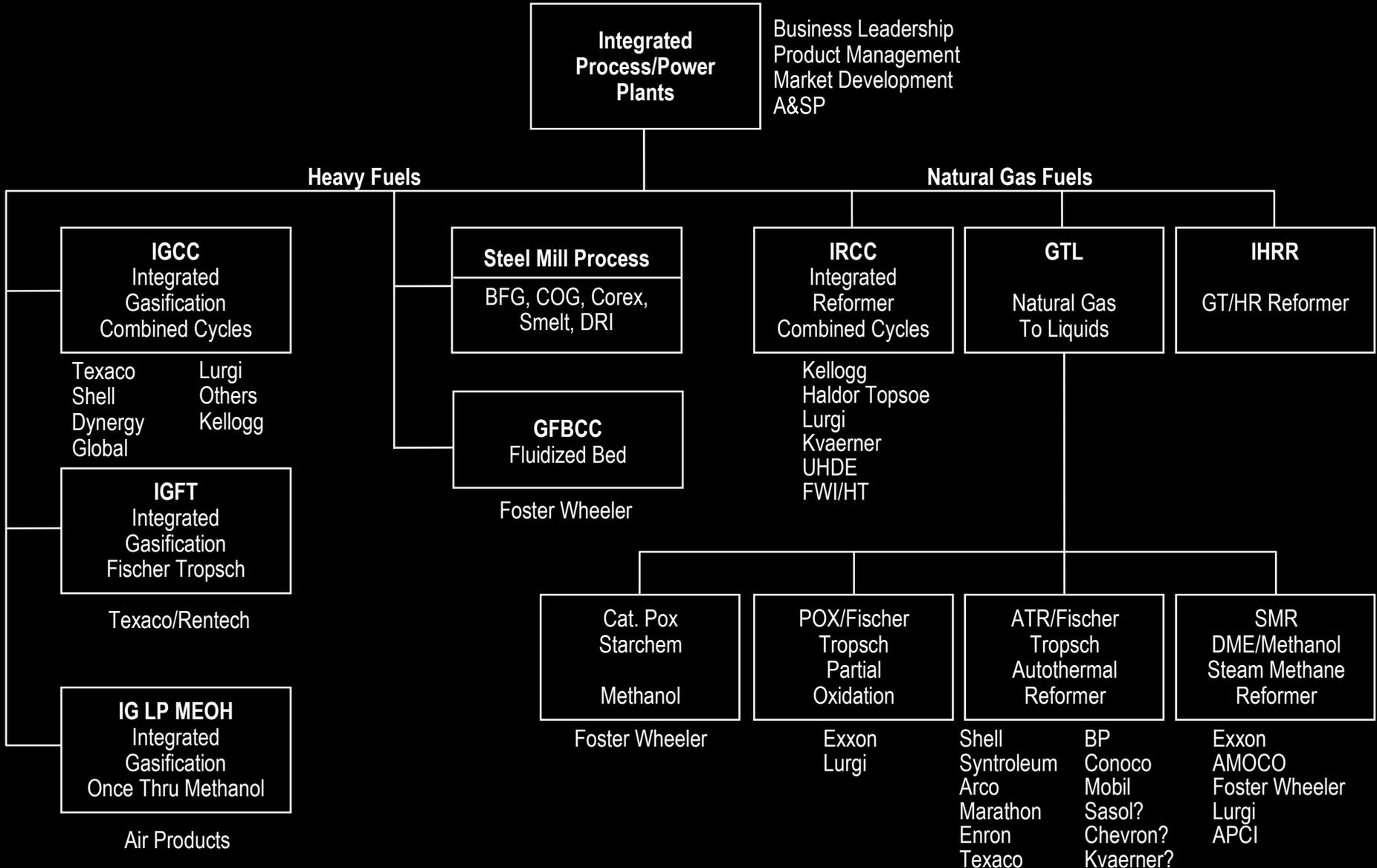
Douglas M. Todd

GE Schenectady, NY

September 19, 2000

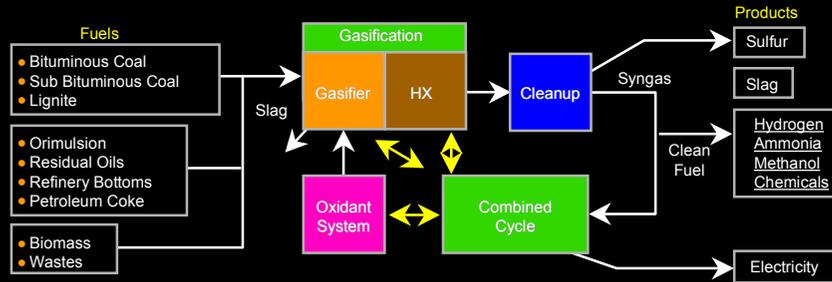


Process Power Plants



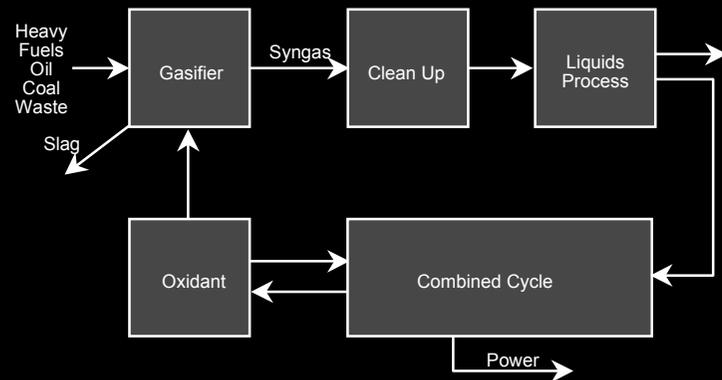
Process Power Plants Examples

IGCC



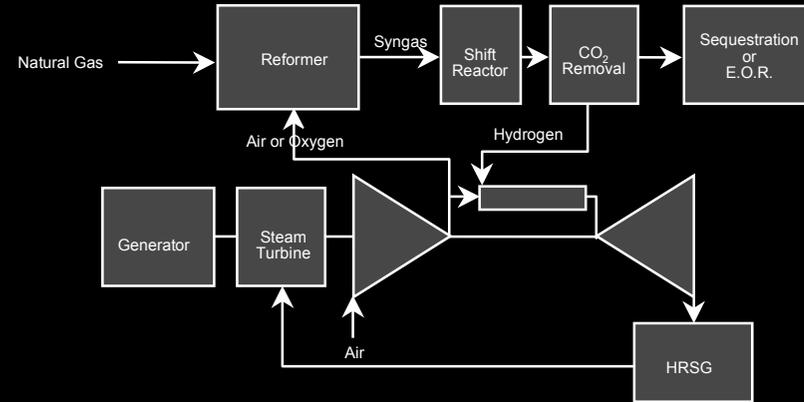
Clean Power From Heavy Fuels

IGFT / Methanol



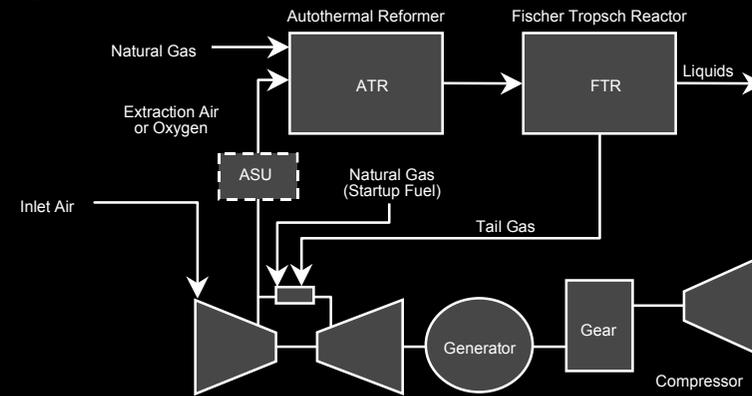
Enhanced IGCC Economics

IRCC



CO₂ Reduction

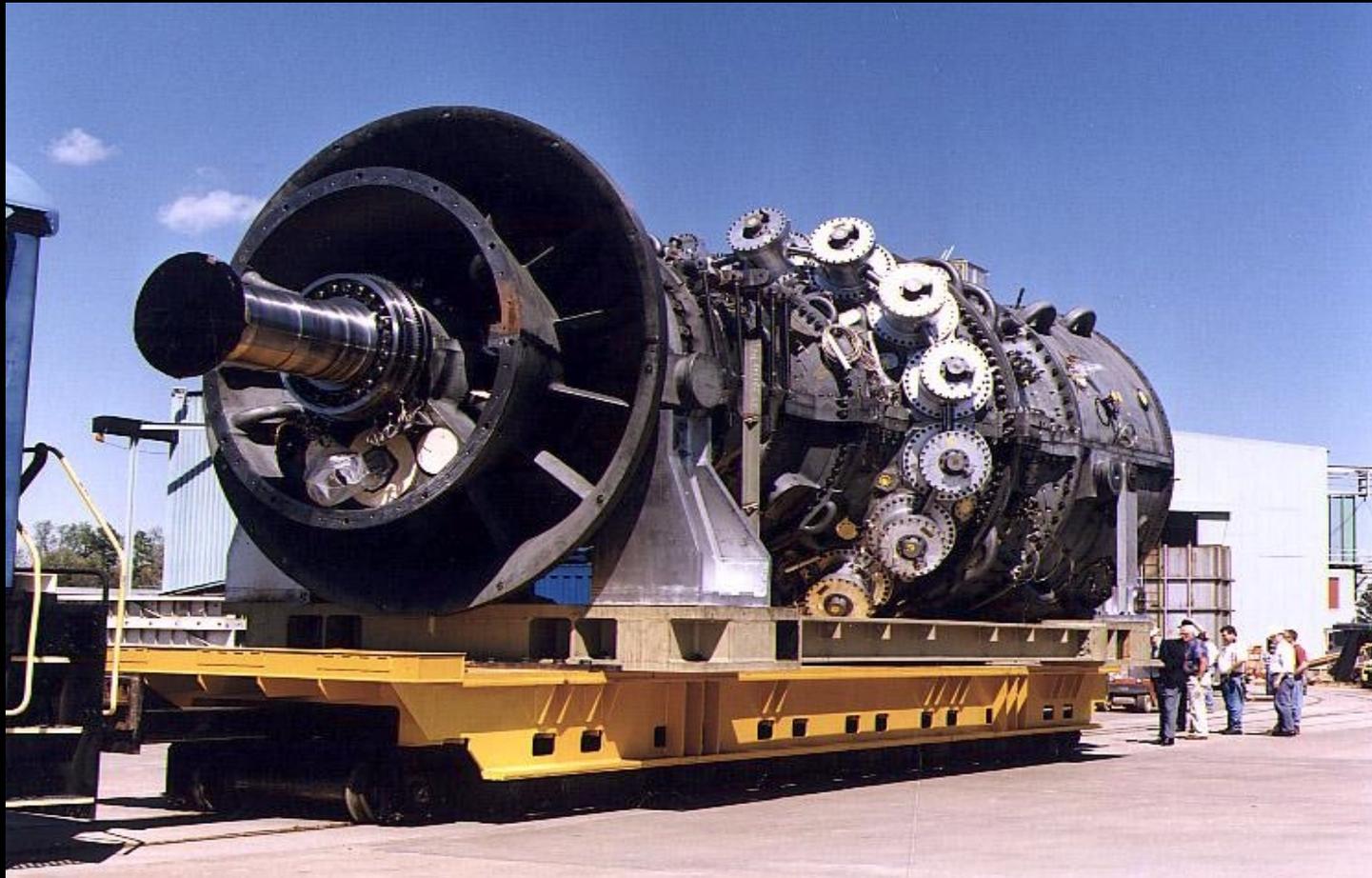
GTL



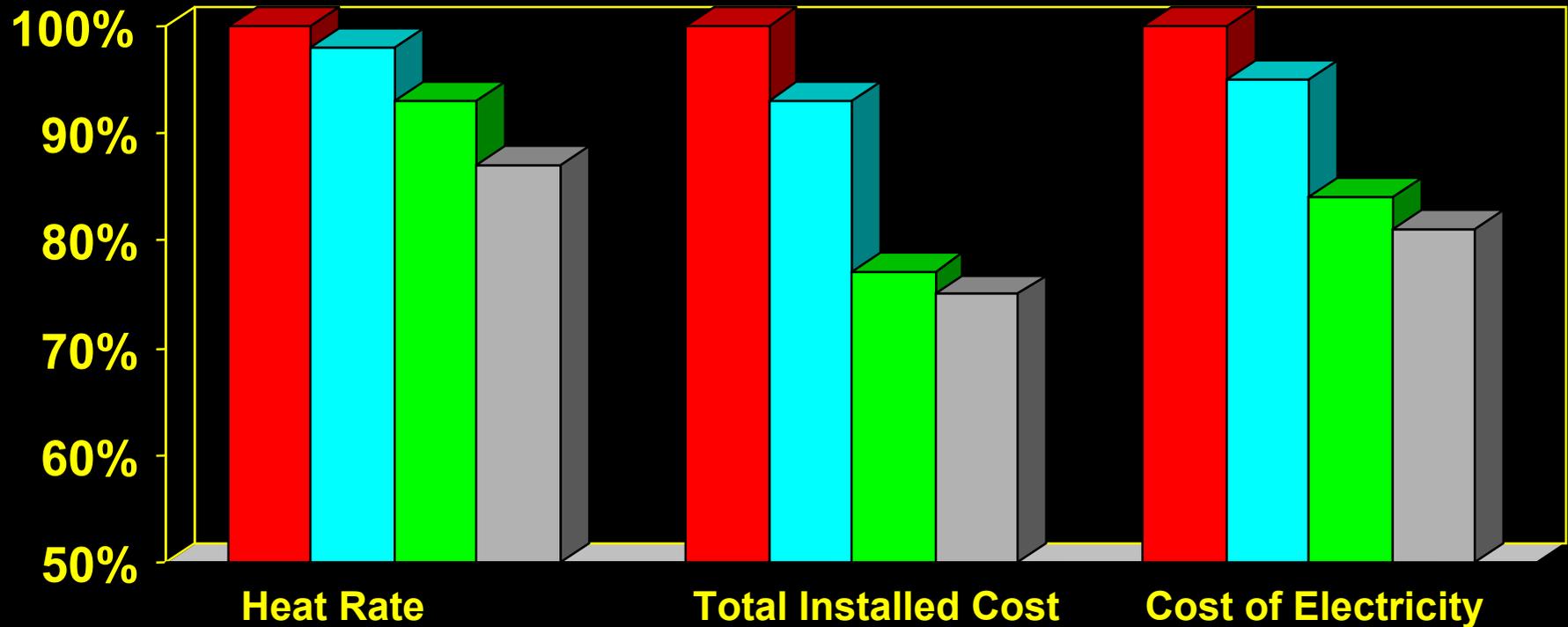
Monetizing Remote Gas

e

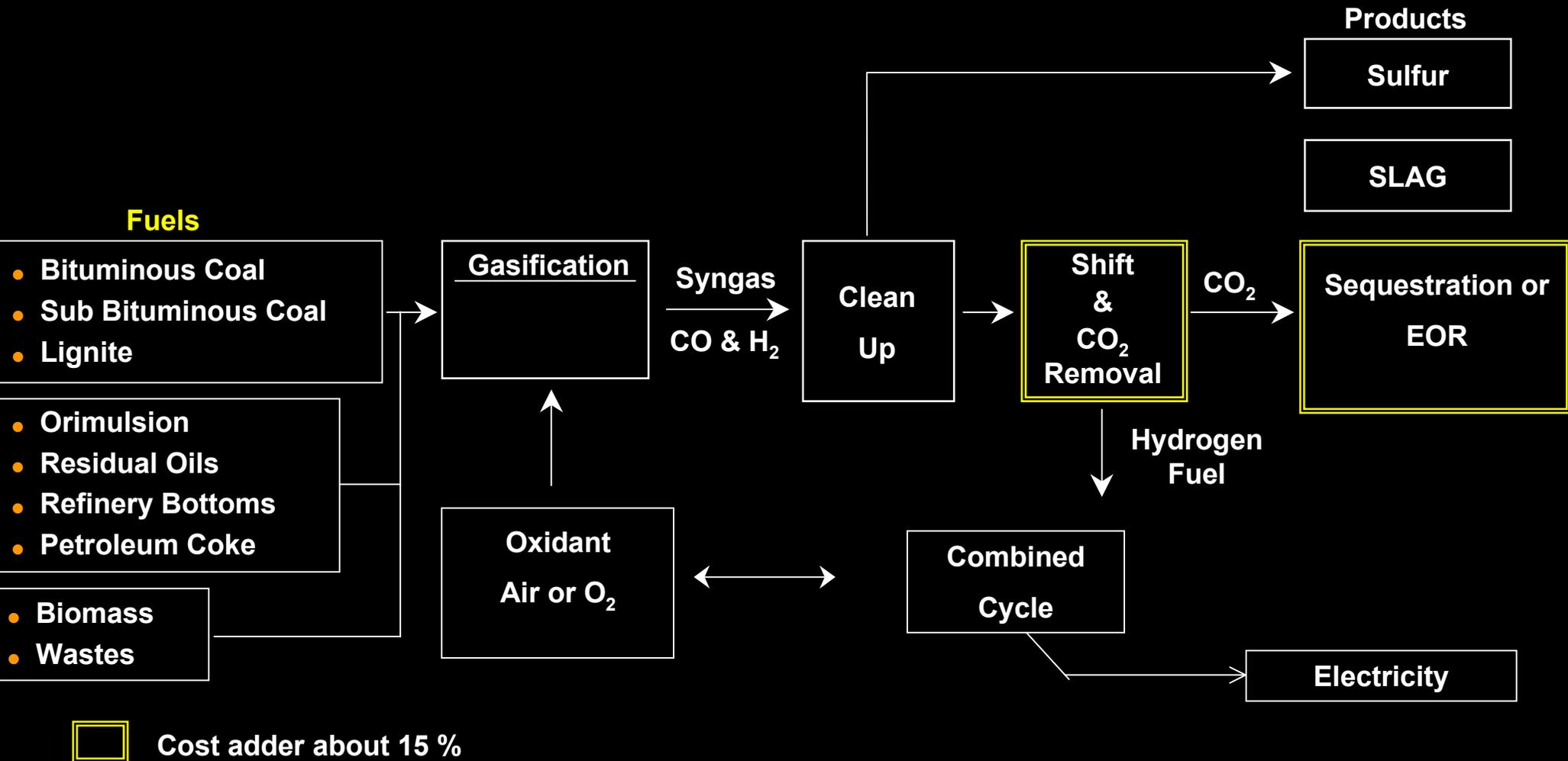
GE's MS9001H Gas Turbine



Economic Impact of HEQ IGCC Design Study Improvements



■ 1994 9F HEQ ■ 1999 9H HEQ
■ 1997 9FA HEQ ■ 1999 9H HR Oil



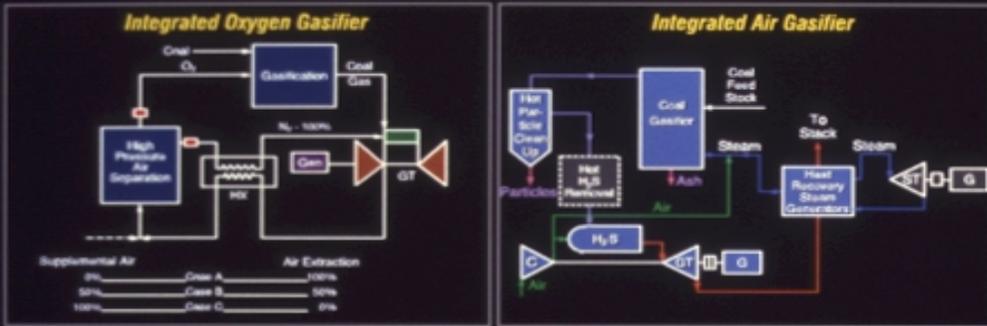
CO₂ Emission Reduction for Heavy Fuel Power Plants

IGCC Penetration

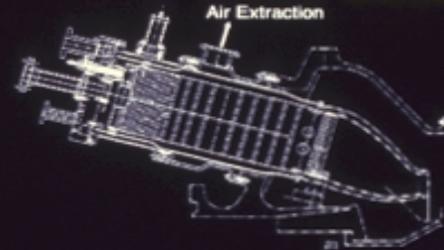
| <u>Customer</u> | <u>C.O. Date</u> | <u>MW</u> | <u>Application</u> | <u>Gasifier</u> |
|-----------------------------------|------------------|------------|--------------------------------------|-------------------------------|
| SCE Cool Water - USA | 1984 | 120 | Power/Coal | Texaco - O₂ |
| LGTI - USA | 1987 | 160 | Cogen/Coal | Destec - O ₂ |
| Demkolec - Netherlands | 1994 | 250 | Power/Coal | Shell - O ₂ |
| PSI/Destec - USA | 1995 | 260 | Repower/Coal | Destec - O₂ |
| Tampa Electric - USA | 1996 | 260 | Power/Coal | Texaco - O₂ |
| Texaco El Dorado - USA | 1996 | 40 | Cogen/Pet Coke | Texaco - O₂ |
| SUV - Czech. | 1996 | 350 | Cogen/Coal | ZUV - O₂ |
| Schwarze Pumpe - Germany | 1996 | 40 | Power/Methanol/Lignite | Noell - O₂ |
| Shell Pernis - Netherlands | 1997 | 120 | Cogen/H₂/Oil | Shell - O₂ |
| Puertollano - Spain | 1998 | 320 | Power/Coal/Pet Coke | Prenflow - O ₂ |
| Sierra Pacific - USA | 1998 | 100 | Power/Coal | KRW - Air |
| ISAB - Italy | 1999 | 500 | Power/H ₂ /Oil | Texaco - O ₂ |
| API - Italy | 2000 | 250 | Power/H ₂ /Oil | Texaco - O ₂ |
| MOTIVA - Delaware | 2000 | 240 | Repower/Pet Coke | Texaco - O₂ |
| Sarlux/Enron - Italy | 2000 | 550 | Cogen/H₂/Oil | Texaco - O₂ |
| EXXON - Singapore | 2002 | 180 | Cogen/H₂/Oil | BGL - O₂ |
| Bio Electrica - Italy | 2000 | 180 | Power/Biomass | Texaco - O₂ |
| FIFE - Scotland | 2000 | 12 | Power/H₂/Cogen/Oil | Lurgi - Air |
| EDF - Total | 2003 | 400 | Power/Sludge | Texaco - O₂ |
| FIFE Electric - Scotland | 2003 | 400 | Power/Coal/RDF | BGL - O₂ |
| Nihon Sekiyu - Japan | 2004 | 350 | Power/Oil | Texaco - O ₂ |
| IOC Paradip | 2004 | 180 | Power/Pet Coke | Shell - O₂ |
| CONFIDENTIAL | 2004 | 750 | Power/Pet Coke | Texaco - O₂ |
| PIEMSA | 2004 | 800 | Power/H₂/Oil | Texaco - O₂ |

GE IGCC Development Program

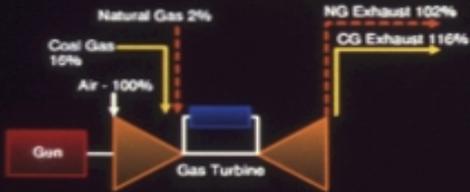
Systems



Combustion

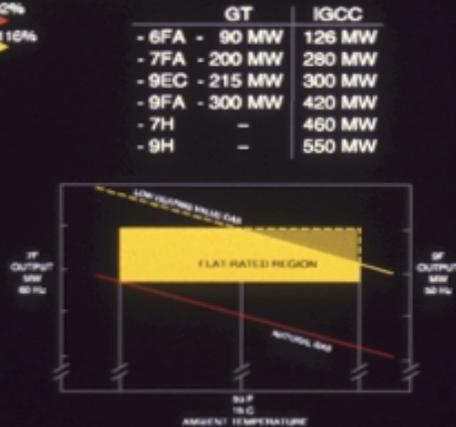


Rating Enhancements



• 14% Difference in Flow at Same Firing Temperature Makes 28% More Output (No Compression Power)

20% Extra Output

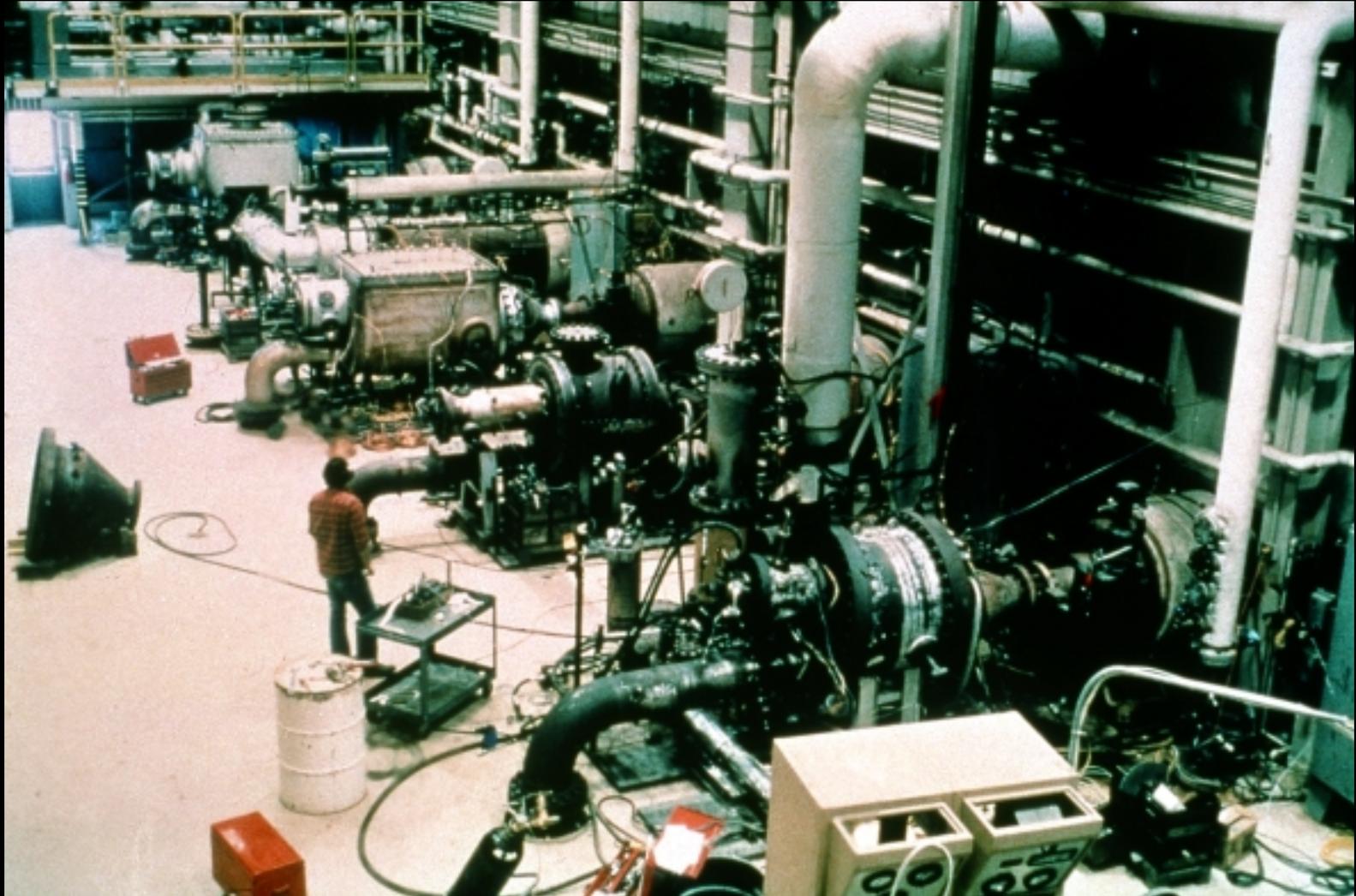


Next Generation



| | Single Train IGCC Plants | |
|--------------|--------------------------|------------------|
| | S107H (60 Hz) | S109H (50 Hz) |
| Net Output | 460 MW | 550 MW |
| Thermal Eff. | 50% | 50% |

GE PGE Combustion Laboratory



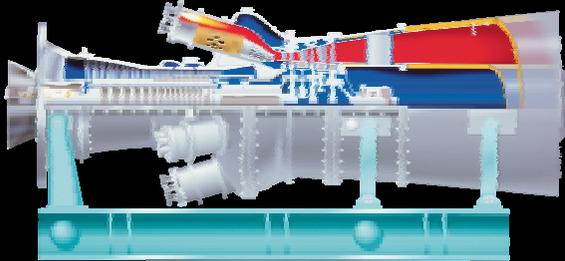
Syngas Comparison

| Syngas | PSI | Tampa | El Dorado | Pernis | Sierra Pacific | ILVA | Schwarze Pumpe | Sarlux | Fife | Exxon Singapore | Motiva Delaware | Confidential | PIEMSA | Tonghua |
|----------------------------|---------|----------------|-----------------------|--------|----------------|---------|----------------|----------|------------------|-----------------|---------------------------------|----------------------------------|----------------|---------|
| H ₂ | 24.8 | 37.2 | 35.4 | 34.4 | 14.5 | 8.6 | 61.9 | 22.7 | 34.4 | 44.5 | 32.0 | 33.34 | 42.3 | 10.3 |
| CO | 39.5 | 46.6 | 45.0 | 35.1 | 23.6 | 26.2 | 26.2 | 30.6 | 55.4 | 35.4 | 49.5 | 42.44 | 47.77 | 22.3 |
| CH ₄ | 1.5 | 0.1 | 0.0 | 0.3 | 1.3 | 8.2 | 6.9 | 0.2 | 5.1 | 0.5 | 0.1 | 0.06 | 0.08 | 3.8 |
| CO ₂ | 9.3 | 13.3 | 17.1 | 30.0 | 5.6 | 14.0 | 2.8 | 5.6 | 1.6 | 17.9 | 15.8 | 17.76 | 8.01 | 14.5 |
| N ₂ + AR | 2.3 | 2.5 | 2.1 | 0.2 | 49.3 | 42.5 | 1.8 | 1.1 | 3.1 | 1.4 | 2.15 | 5.72 | 2.05 | 48.2 |
| H ₂ O | 22.7 | 0.3 | 0.4 | -- | 5.7 | -- | -- | 39.8 | -- | 0.1 | 0.44 | 0.08 | 0.15 | 0.9 |
| LHV, - Btu/ft ³ | 209 | 253 | 242 | 210 | 128 | 183 | 317 | 163 | 319 | 241 | 248 | 230.4 | 270.4 | 134.6 |
| - kJ/m ³ | 8224 | 9962 | 9528 | 8274 | 5024 | 7191 | 12,492 | 6403 | 12,568 | 9,477 | 9,768 | 9,079 | 10,655 | 5304 |
| T _{fuel} F/C | 570/300 | 700/371 | 250/121 | 200/98 | 1000/538 | 400/204 | 100/38 | 392/200 | 100/38 | 350/177 | 570/299 | 300/149 | 338/170 | - |
| H ₂ /CO Ratio | .63 | .80 | .79 | .98 | .61 | .33 | 2.36 | .74 | .62 | 1.26 | .65 | .79 | .89 | .46 |
| Diluent | Steam | N ₂ | N ₂ /Steam | Steam | Steam | -- | Steam | Moisture | H ₂ O | Steam | H ₂ O/N ₂ | N ₂ /H ₂ O | N ₂ | n/a |
| Equivalent LHV | | | | | | | | | | | | | | |
| - Btu/ft ³ | 150 | 118 | 113* | 198 | 110 | -- | 200 | -- | * | 116 | 150 | 115.3 | 129 | 134.6 |
| - kJ/m ³ | 5910 | 4649 | 4452 | 7801 | 4334 | -- | 7880 | -- | -- | 4600 | 5910 | 4543 | 5083 | 5304 |

* Always co-fired with 50% natural gas

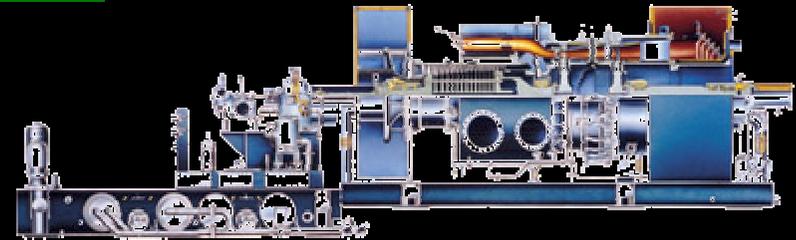
Combustion Technology Development

IGCC



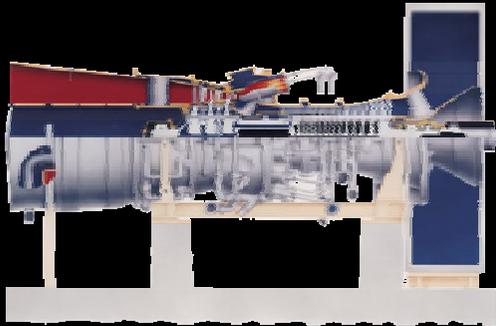
MOTIVA - First Pet Coke Appli. With 9 ppm NO_x
Exxon - 1st St. Cracker Bottoms With 25% Wobbe Var.

GTL



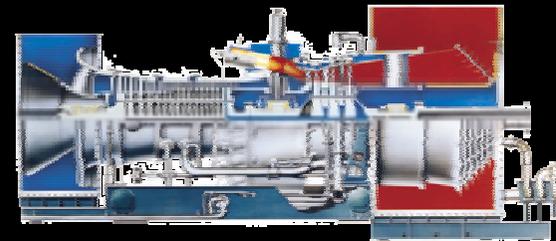
Air - First Air-Blown Tail Gas
Oxygen - Variety of Syngas

IRCC



Hydrogen Combustion for Reduction of CO₂

Steel



Mixtures of BFG, COG, Nat. Gas

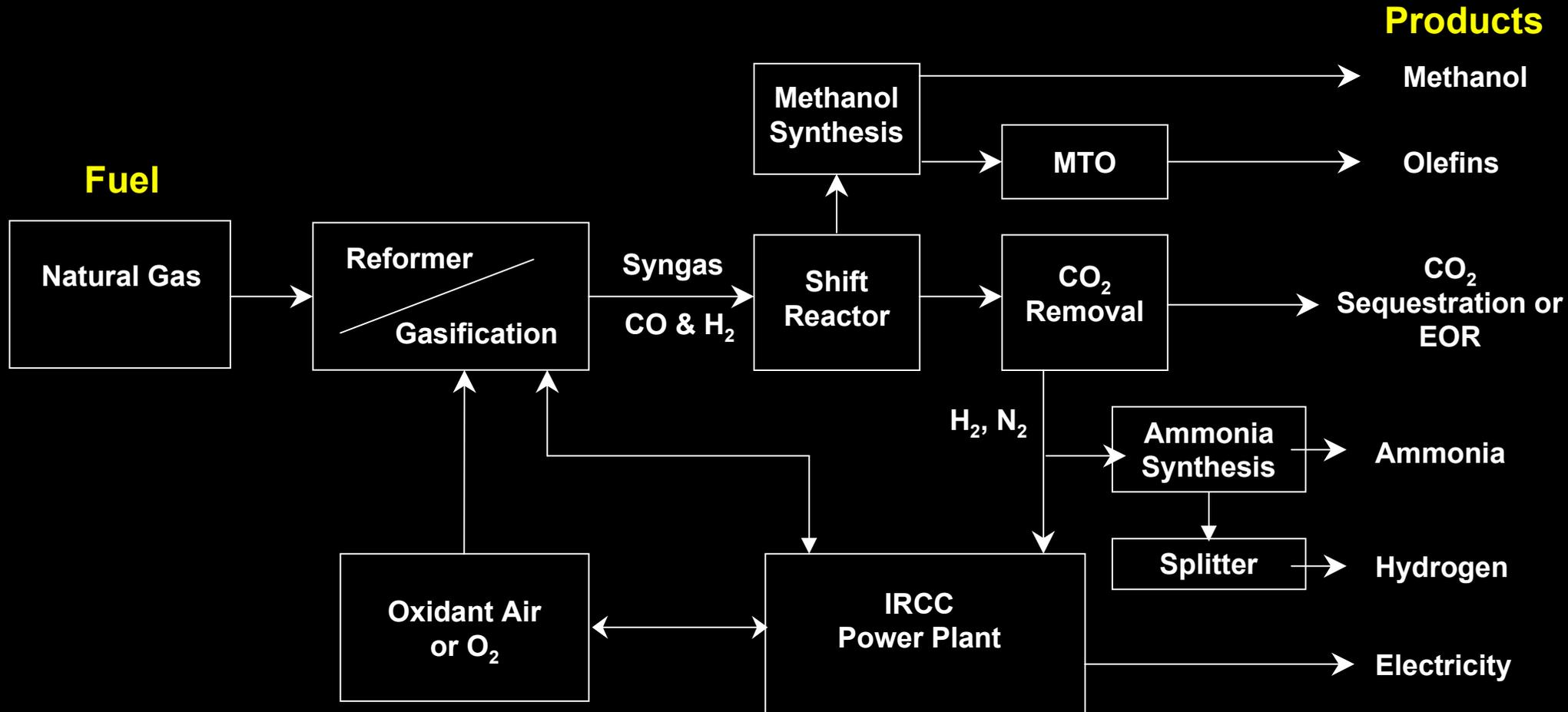
Shell-Pernis Coproduction Plant

- 1650 t/d Vacuum Residue
- 2 x 6B Gas Turbines
- Shell/Lurgi Gasifier
- 255 t/d Hydrogen
- 115 MW Power
- Steam to Refinery
- Operation 1997



RDC 27963

IRCC Electricity Coproduction

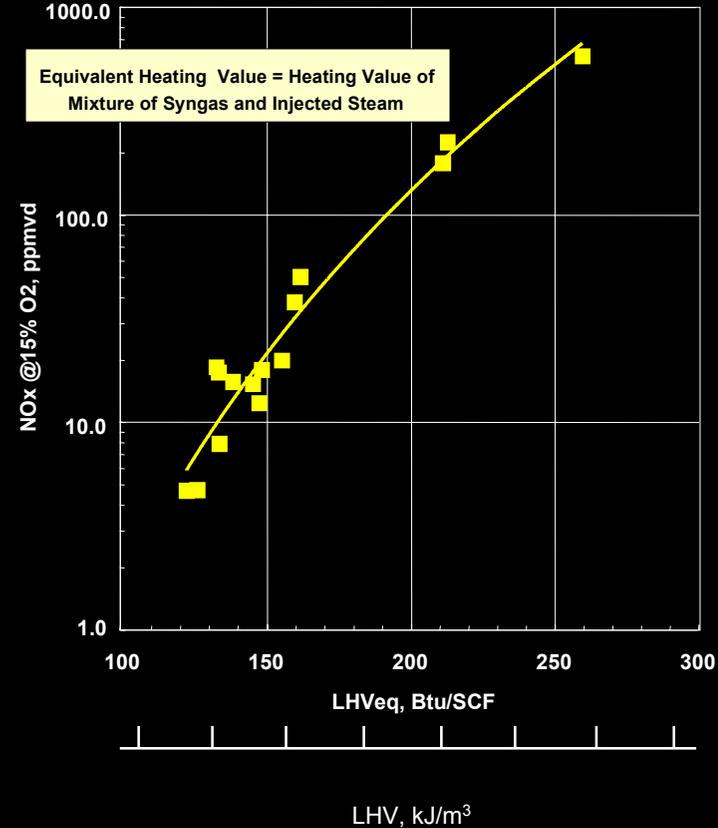


**Multiple Products and Electricity with
CO₂ Emission Reduction from Natural Gas**

Combustion Test Objectives

- Evaluate Operability and Emissions of the GE IGCC Multi-Nozzle Combustor burning IRCC High H₂ Fuel
- Evaluate Component Metal Temperatures Throughout the Load Range
- Determine Sensitivity of Major Performance Parameters to Variations in Hydrogen Content

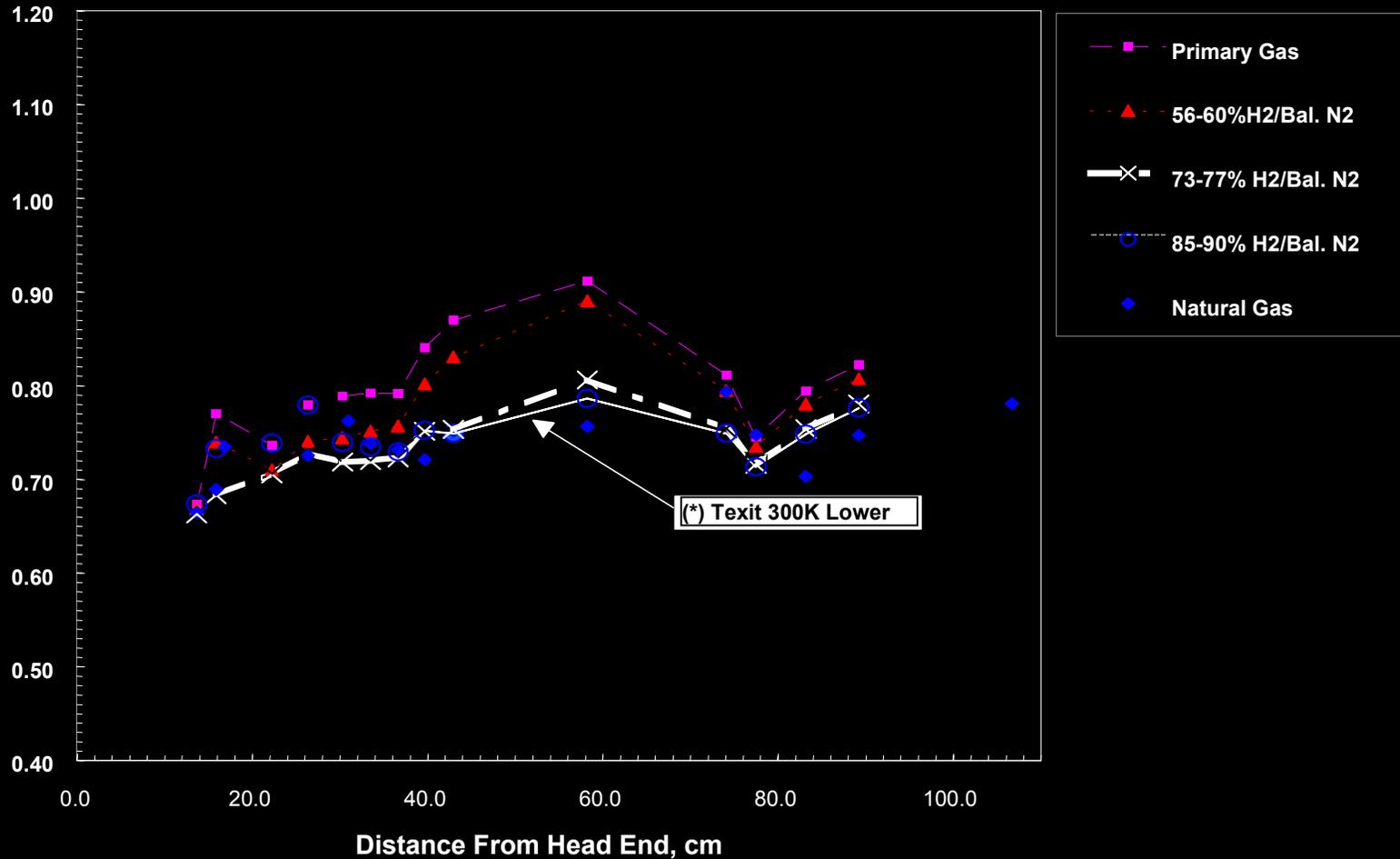
NOx vs Equivalent Calorific Value for Several Fuel Compositions



50 - 95% H₂ By Volume, Bal. N₂, N₂ + H₂O

e

Combustor Metal Temperatures at 210° from TDC - Inline with Fuel Nozzles

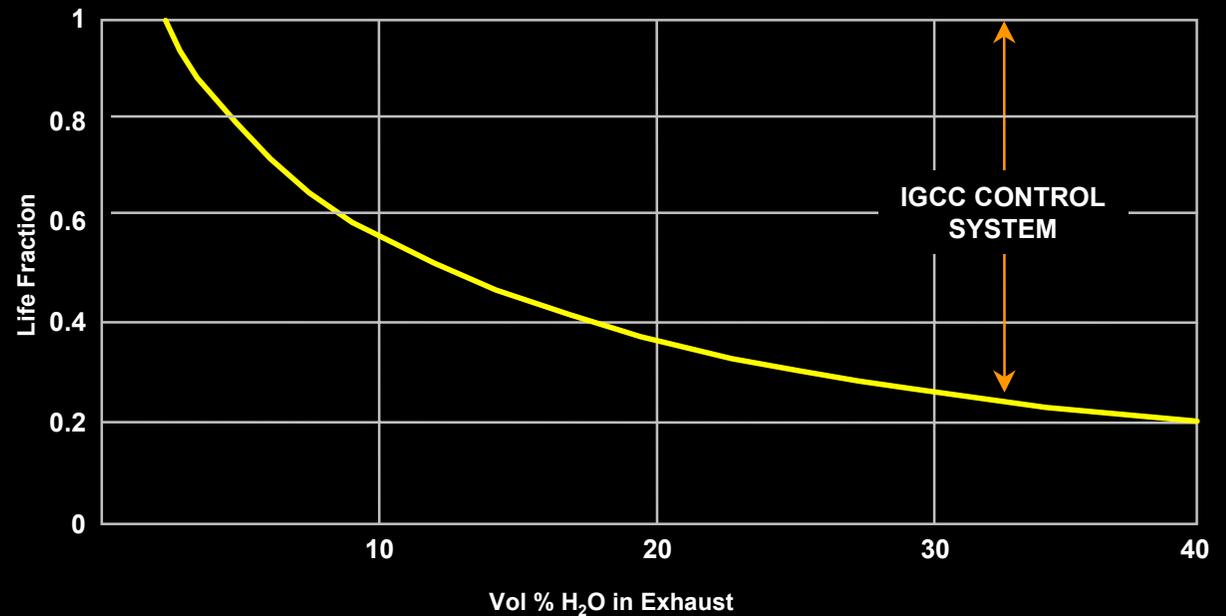


Effect of Fuel Composition on Axial Metal Temperature Distribution at 210° from TDC

Syngas - Reliability / Availability / Maintenance

Syngas Combined Cycle Can Have Same Performance as Natural Gas Combined Cycle

- Need Automatic Fuel Switch/Nitrogen Purge
- Need Clean Syngas
- Reduced Firing Temp to Maintain Design Metal Temp/ 100% Life



Conclusions

- Hydrogen is an acceptable fuel for GE Gas Turbines using IGCC Combustors
- NO_x Emissions Below 10 ppmvd @15% O₂
- No Adverse Effects on Combustion Parts Lives
- Reliability, Availability and Maintainability Equivalent to NG
- Integration of a Hydrogen Fueled Gas Turbine with Process Plants is Technically Feasible to Reduce CO₂ Emissions by 90%
- Optimization Required to Improve Cost of Electricity